

THE DETERMINATION OF THE MOST PROBABLE MECHANISM FUNCTION AND THREE KINETIC PARAMETERS OF EXOTHERMIC DECOMPOSITION REACTION OF ENERGETIC MATERIALS BY A SINGLE NON-ISOTHERMAL DSC CURVE *

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ABSTRACT

The determination of the most probable mechanism function and a numerical method of computing three kinetic parameters (The activation energy (E), the pre-exponential constant (A) and the reaction order (n)) of exothermic decomposition reaction of energetic materials by a single non-isothermal DSC curve obtained with a model CDR-1 instrument with a scaled cell of stainless steel and an open cell of aluminium are reported. The data are fitted to the integral, differential and exothermic rate equations by linear least-squares, iterative, combined dichotomous and least-squares methods, respectively. After establishing the most probable general expression of differential or integral mechanism functions by the logical choice method, the corresponding values of E , A and n will be obtained by the exothermic rate equation.

INTRODUCTION

The apparent activation energy, pre-exponential constant and reaction order are three important parameters from the point of view of the evaluation of stability and compatibility for energetic materials [1–3]. The determination of the most probable mechanism function and three kinetic parameters of exothermic decomposition reaction of energetic materials at the same time by a single non-isothermal DSC curve has never been reported before. In this paper, these kinetic parameters and a mechanism function were obtained from the calculation of a single DSC curve by the integral, differential and exothermic rate equations. This is quite useful for us in the analysis and study of stability and compatibility of energetic materials.

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EXPERIMENTAL

Materials

The 2,6-dinitrophenol (I) used was of analytical purity. It was a commercial product of the Beijing Chemical Engineering Factory. The purified 1,4,5,8-tetranitro 1,4,5,8-tetrazadelin (II), cast single-base propellant (III, 99% nitrocellulose, 1% methyl centralite) and double-base propellant (IV, 60.3% nitrocellulose, 29.9% nitroglycerine, 8.3% triacetin and 1.5% methyl centralite) were prepared by our Institute.

Experimental equipment and conditions

DSC experiments of above-mentioned materials were carried out on a Shanghai Balance Manufacturers' CDR-1 differential scanning calorimeter, using a Ni/Cr–Ni/Si thermoelement and working under static ambient conditions at a heating rate of 5 or 10°C min⁻¹. DSC curves were obtained for both the sealed cell of stainless steel (Fig. 1) and the open cell of aluminium. Heat-treated α -Al₂O₃ was used as reference sample: the sample weight varied in the range 1.5–2.5 mg. Sensitivity and paper speed were 41.84 mJ s⁻¹ and 20 mm min⁻¹ respectively. Heating rate ϕ was calculated according to the actual rising rate of temperature from 50°C to the temperature at the end of reaction.

As four typical examples for energetic materials, the DSC curves of exothermic decomposition reaction of the samples I, II, III and IV are shown in Fig. 2. The DSC curve of I was obtained with the sealed cell; the DSC curves of the others were obtained with the open cell.

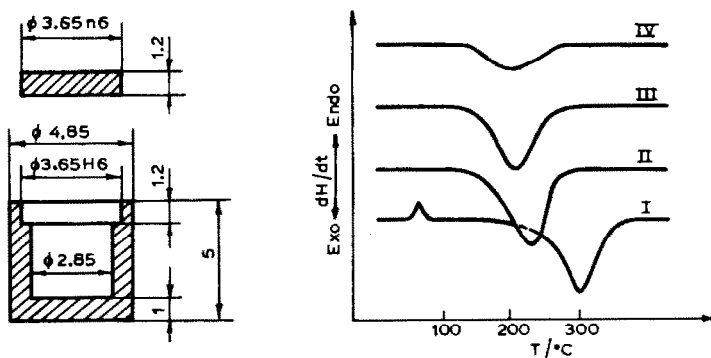


Fig. 1. Sealed cell scheme.

Fig. 2. Typical DSC curves of thermal decomposition of energetic materials I, 2,6-dinitrophenol; II, 1,4,5,8-tetranitro 1,4,5,8-tetrazadelin; III, cast single-base propellant; IV, double-base propellant.

KINETIC EQUATIONS AND ANALYSIS OF KINETIC DATA

In order to analyze kinetic problems, two different equations, i.e., eqns. (1) and (2), are used

$$d\alpha/dt = kf(\alpha) \quad (1)$$

and

$$G(\alpha) = kt \quad (2)$$

where α is the fraction of the material reacted, t is the time and k is the kinetic constant. $f(\alpha)$ and $G(\alpha)$ are differential and integral mechanism functions, respectively. The relationship between $f(\alpha)$ and $G(\alpha)$ is given by

$$f(\alpha) = \frac{1}{G'(\alpha)} = \frac{1}{d[G(\alpha)]/d\alpha} \quad (3)$$

The relationship between the kinetic constant (k) and the absolute temperature (T) of reaction is expressed by the well-known Arrhenius equation

$$k = A \exp(-E/RT) \quad (4)$$

It is believed that eqns. (1)–(4) are also valid for non-isothermal cases (at least empirically) [4]. In this case, E and A are the derived activation energy and pre-exponential constant, respectively. R is the gas constant.

Setting T_0 as the initial point of the deviation from the baseline of the DSC curve (see Fig. 3) and ϕ as the constant heating rate, we have

$$T = T_0 + \phi t \quad (5)$$

In order to obtain an overall relationship for non-isothermal kinetics, eqns. (2), (4) and (5) are combined to yield

$$G(\alpha) = \frac{A}{\phi} (T - T_0) e^{-E/RT} \quad (6)$$

Taking logarithm on both sides of the eqn. (6), the integral equation (eqn. (7)) may be obtained

$$\ln\left(\frac{G(\alpha)}{T - T_0}\right) = \ln\left(\frac{A}{\phi}\right) - \frac{E}{RT} \quad (7)$$

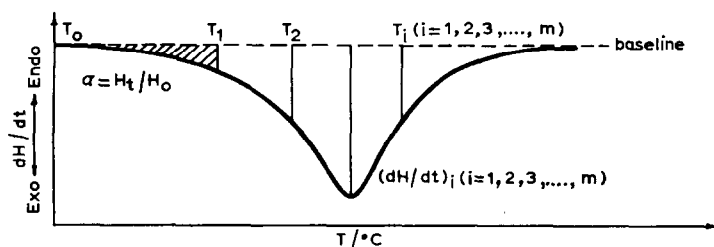


Fig. 3. Schematic diagrams of typical DSC curves of thermal decomposition for energetic materials.

The data are fitted to eqn. (7) by the linear least-squares method on the computer (program IM).

On differentiation, re-arrangement on both sides of the eqn. (6) and recalling eqn. (3), taking logarithms on both sides of the equation, the differential eqn. (8) is obtained

$$\ln \left[\frac{d\alpha/dT}{f(\alpha) \left[E(T - T_0)/RT^2 + 1 \right]} \right] = \ln \frac{A}{\phi} - \frac{E}{RT} \quad (8)$$

Equation (8) may be solved by the iterative method (program DM) on the computer. Any arbitrary value may be assumed for E ($E > 0$), and using this

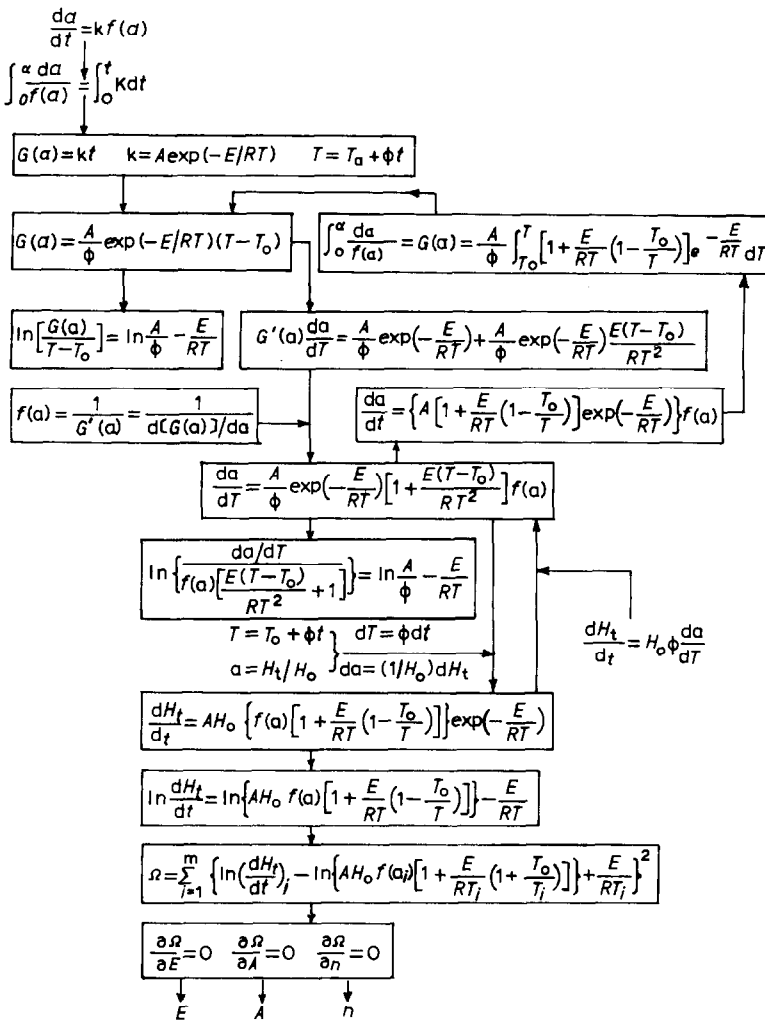


Fig. 4. Different types of kinetic equations for non-isothermal reactions and their derivation process.

value the value of the expression on the left-hand side may be calculated for each data point. This, when plotted against $(1/T)$ by the linear least-squares method, gives new values of E from the slope and A from the intercept. This modified value of E is used as a starting value for the next iteration which yields another modified value of E . Thus after a few iterations, consistent values of E and A will be obtained.

Combining eqns. (3), (5) and (8), we have

$$\frac{d\alpha}{dt} = \left\{ A \left[1 + \frac{E}{RT} \left(1 - \frac{T_0}{T} \right) \right] \exp\left(-\frac{E}{RT}\right) \right\} f(\alpha) \quad (9)$$

Rearranging both sides of eqn. (9) and integrating yields

$$\int_0^\alpha \frac{d\alpha}{f(\alpha)} = G(\alpha) = \frac{A}{\phi} \int_{T_0}^T \left[1 + \frac{E}{RT} \left(1 - \frac{T_0}{T} \right) \right] e^{-E/RT} dT \quad (10)$$

Equation (6) may be also obtained from eqn. (10).

Combining eqn. (9) and $\alpha = H_t/H_0$, we have

$$\frac{dH_t}{dt} = AH_0 \left\{ f(\alpha) \left[1 + \frac{E}{RT} \left(1 - \frac{T_0}{T} \right) \right] \right\} \exp\left(-\frac{E}{RT}\right) \quad (11)$$

where H_0 is the total exothermicity of the substance (corresponding to the global area under the DSC curve) and H_t is the reaction heat in a certain time (corresponding to the partial area under the DSC curve).

Substituting the probable mechanism function obtained logically from the integral and differential methods, for example $f(\alpha) = (1 - \alpha)^n$, into eqn. (11), we have

$$\ln \frac{dH_t}{dt} = \ln \left\{ AH_0 (1 - \alpha)^n \left[1 + \frac{E}{RT} \left(1 - \frac{T_0}{T} \right) \right] \right\} - \frac{E}{RT} \quad (12)$$

Equation (12) is known as the exothermic rate equation [5].

Taking minimal values of evaluation functions (E , A and n)

$$\Omega = \sum_{i=1}^m \left\{ \ln \left(\frac{dH_t}{dt} \right)_i - \ln \left\{ AH_0 (1 - \alpha_i)^n \left[1 + \frac{E}{RT_i} \left(1 - \frac{T_0}{T_i} \right) \right] \right\} + \frac{E}{RT_i} \right\}^2 \quad (13)$$

the following normal equations can be obtained from eqn. (13)

$$\frac{\partial \Omega}{\partial E} = 0 \quad (14)$$

$$\frac{\partial \Omega}{\partial A} = 0 \quad (15)$$

$$\frac{\partial \Omega}{\partial n} = 0 \quad (16)$$

Once the value of E has been calculated from eqn. (14), the corresponding values of A and n can then be obtained from eqns. (15) and (16) by program ETA on the computer. In the iterative computation process of

TABLE 1

Several kinetic functions used for the present analysis

Function No.	Function form ^a (integral form), $G(\alpha)$	
1	α^2	
2	$\alpha + (1 - \alpha) \ln(1 - \alpha)$	
3	$1 - (2/3)\alpha - (1 - \alpha)^{2/3}$	
4-5	$[1 - (1 - \alpha)^{1/3}]^n$	$(n = 2, 1/2)$
6	$[1 - (1 - \alpha)^{1/2}]^{1/2}$	
7	$[(1 + \alpha)^{1/3} - 1]^2$	
8	$[(1/(1 - \alpha))^{1/3} - 1]^2$	
9	$-\ln(1 - \alpha)$	
10-16	$[-\ln(1 - \alpha)]^n$	$(n = 2/3, 1/2, 1/3, 4, 1/4, 2, 3)$
17-22	$1 - (1 - \alpha)^n$	$(n = 1/2, 3, 2, 4, 1/3, 1/4)$
23-27	α^n	$(n = 1, 3/2, 1/2, 1/3, 1/4)$
28	$(1 - \alpha)^{-1}$	
29	$(1 - \alpha)^{-1} - 1$	
30	$(1 - \alpha)^{-1/2}$	

^a Differential form, $f(\alpha) = 1/G'(\alpha)$.

combined dichotomous and least-squares methods, we take $AA = 10^{-1}$, $BB = 10^{10}$, $H = 50.0$, $E_1 = 10^{-10}$ and $E_2 = 10^{-5}$, where E is the root of eqn. (14). $[AA, BB]$ is the root interval of eqn. (14). H is the step size and E_1 and E_2 are two constants of the control precision. When the value of a certain point on the left side of the eqn. (14) is less than E_1 or a half of the little interval length is less than E_2 , this point or the intermediate point of the little interval is the solution of eqn. (14). Figure 4 shows a block diagram of

TABLE 2

Data of cast single-base propellant determined by DSC

Data point	T_i (K)	α_i	$(dH_i/dt)_i$ (mJ s ⁻¹)	$(d\alpha/dT)_i \times 10^3$ (K ⁻¹)
1	456.2	0.0190	0.9791	5.360
2	458.2	0.0380	1.674	9.163
3	461.2	0.0640	2.427	13.29
4	464.2	0.1070	3.205	17.54
5	465.2	0.1300	3.757	20.57
6	467.2	0.1590	4.435	24.28
7	468.2	0.1920	5.322	29.14
8	470.2	0.2350	6.636	36.33
9	472.2	0.2840	8.301	45.45
10	473.2	0.3530	9.849	53.92
11	474.2	0.4240	10.74	58.82
12	477.2	0.5070	11.08	60.66

 $T_0 = 448.2$ K; $H_0 = 2119$ mJ; $\phi = 0.0862$ °C s⁻¹.

TABLE 3

Results of analysis of the thermal decomposition data of cast single-base propellant by integral (eqn. (7)) and differential (eqn. (8)) methods

Function No.	Integral method				Differential method			
	E (kJ mol ⁻¹)	$\log A$ (s ⁻¹)	r	Q	E (kJ mol ⁻¹)	$\log A$ (s ⁻¹)	r	Q
1	437.44	44.9	0.988	0.687458	406.13	41.5	0.989	0.534294
2	453.95	46.5	0.990	0.615434	431.25	44.0	0.992	0.433544
3	459.84	46.5	0.990	0.591121	440.24	44.4	0.993	0.403690
4	471.65	47.8	0.992	0.547196	457.95	46.4	0.994	0.359185
5	36.79	1.15	0.968	0.012904	65.96	4.41	0.951	0.066142
6	34.59	1.00	0.967	0.011801	60.82	3.92	0.950	0.057707
7	414.00	41.2	0.985	0.772153	373.42	36.8	0.984	0.644560
8	508.35	52.0	0.994	0.450655	511.29	52.4	0.996	0.330448
9	190.76	18.2	0.993	0.078635	202.38	19.5	0.992	0.099703
10	91.12	7.35	0.989	0.026169	116.04	10.1	0.978	0.088000
11	41.29	1.91	0.969	0.015934	76.38	5.81	0.950	0.091266
12	-ve	-ve	0.624	0.016364	40.38	1.84	0.837	0.100849
13	1087.5	116	0.993	2.470571	1072.7	114	0.994	1.837605
14	-ve	-ve	0.942	0.020578	24.06	0.05	0.662	0.108899
15	489.68	50.8	0.993	0.491999	484.43	50.3	0.995	0.325442
16	788.61	83.5	0.993	1.289312	777.04	82.3	0.995	0.896243
17	177.35	16.4	0.990	0.087633	177.84	16.5	0.991	0.081851
18	120.49	10.7	0.957	0.191892	64.60	4.59	0.697	0.635448
19	141.26	12.8	0.976	0.145320	107.47	9.21	0.924	0.282975
20	102.10	8.72	0.930	0.234640	26.60	0.47	0.286	1.161563
21	181.74	16.7	0.991	0.083795	185.97	17.2	0.992	0.083168
22	183.96	16.8	0.992	0.082174	190.06	17.5	0.992	0.085569
23	164.63	15.2	0.987	0.103134	153.77	14.1	0.985	0.105989
24	301.03	30.0	0.988	0.328995	276.94	27.4	0.988	0.262071
25	28.24	0.42	0.960	0.009876	45.75	2.39	0.926	0.049928
26	-ve	-ve	0.915	0.008257	16.18	-ve	0.662	0.051478
27	-ve	-ve	0.973	0.012972	3.89	-ve	0.166	0.056700
28	-ve	-ve	0.789	0.231331	252.56	25.2	0.986	0.258986
29	219.68	21.5	0.994	0.090291	252.56	25.2	0.986	0.258986
30	-ve	-ve	0.941	0.121445	227.31	22.1	0.989	0.158928

TABLE 4

Data of double-base propellant determined by DSC

Data point	T_i (K)	α_i	$(dH_i/dt)_i$ (mJ s ⁻¹)	$(d\alpha/dT)_i \times 10^3$ (K ⁻¹)
1	448.2	0.0176	0.4100	4.108
2	454.2	0.0441	0.9205	9.222
3	458.2	0.0969	1.799	18.02
4	461.2	0.1322	2.159	21.63
5	463.2	0.1806	2.611	26.16
6	466.2	0.2555	3.347	33.53
7	467.2	0.2996	3.582	35.88
8	468.2	0.3480	4.008	40.16
9	470.2	0.3921	4.100	41.08
10	471.2	0.4405	4.276	42.84

$T_0 = 441.2$ K; $H_0 = 1140$ mJ; $\phi = 0.0876$ °C s⁻¹.

TABLE 5

Data of 1,4,5,8-tetranitro 1,4,5,8-tetrazadecalin determined by DSC

Data point	T_i (K)	α_i	$(dH_i/dt)_i$ (mJ s ⁻¹)	$(d\alpha/dT)_i \times 10^3$ (K ⁻¹)
1	477.2	0.0145	0.3314	2.429
2	485.2	0.0253	0.5556	4.073
3	487.2	0.0393	0.9037	6.624
4	490.2	0.0556	1.228	9.004
5	493.2	0.0857	1.918	14.6
6	495.2	0.1190	2.634	19.31
7	497.2	0.1654	3.769	27.63
8	499.2	0.2332	5.295	38.81
9	500.2	0.3064	6.823	50.05
10	502.2	0.3904	8.485	62.19
11	503.2	0.5164	9.864	72.30
12	504.2	0.6133	10.73	78.68
13	505.2	0.6942	11.20	82.09
14	506.2	0.7868	11.34	83.12
15	507.2	0.8740	10.50	76.99

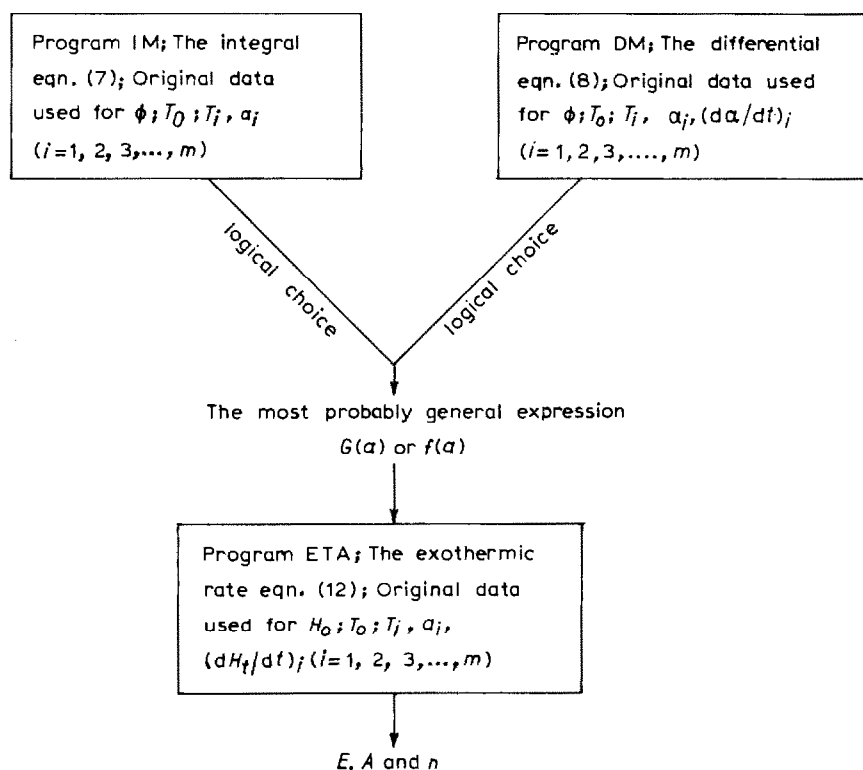
 $T_0 = 471.2 \text{ K}; H_0 = 1554 \text{ mJ}; \phi = 0.0878 \text{ } ^\circ\text{C s}^{-1}$


Fig. 5. Block diagram of the process of computing three kinetic parameters.

above-mentioned different types of kinetic equations for non-isothermal reactions and their derived process. For example, using all the forms of $G(\alpha)$ and $f(\alpha)$ as tabulated in Table 1, the data of cast single-base propellant tabulated in Table 2, are analyzed by eqns. (7) and (8). The results obtained from Table 3 clearly show that when all conditions (viz. the values of E and A are in the ordinary range of the thermal decomposition kinetic parameters for energetic materials ($E = 80\text{--}250 \text{ kJ mol}^{-1}$; $\log A = 7\text{--}30 \text{ s}^{-1}$, linear correlation coefficient $r > 0.99$ and variance $Q < 0.1$) are satisfied at the same time the probable mechanism function is logically function No. 9, 17, 21 and 22. Their general expression is $f(\alpha) = (1 - \alpha)^n$. By substituting the most probable mechanism function into the exothermic rate eqn. (12), the proper values of E , A and n are determined thereafter by eqns. (14)–(16). The value of E for sample III is in good agreement with the

TABLE 6

Data of 2,6-dinitrophenol determined by DSC with the sealed cell of stainless steel. Traces 1 and 2

Data point	T_i (K)	α_i	$(dH_i/dt)_i$ (mJ s ⁻¹)	$(d\alpha/dT)_i \times 10^3$ (K ⁻¹)
1	522.2	0.0073	0.9774	0.8484
2	534.2	0.0249	2.721	2.362
3	542.2	0.0484	4.398	3.818
4	549.2	0.0822	7.223	6.270
5	554.2	0.1174	9.921	8.612
6	560.2	0.1809	13.87	12.04
7	564.2	0.2315	18.02	15.65
8	569.2	0.3098	24.33	21.12
9	574.2	0.4095	32.43	28.16
10	577.2	0.5014	38.26	33.21
11	580.2	0.5869	42.14	36.58
12	582.2	0.6596	43.10	37.41

$T_0 = 503.2 \text{ K}$; $H_0 = 6843 \text{ mJ}$; $\phi = 0.1683 \text{ }^\circ\text{C s}^{-1}$

1	521.2	0.0061	0.9774	0.8632
2	534.2	0.0223	2.721	2.403
3	542.2	0.0452	4.398	3.885
4	549.2	0.0783	7.223	6.380
5	555.2	0.1135	9.921	8.762
6	560.2	0.1608	13.87	12.25
7	564.2	0.2131	18.02	15.92
8	568.2	0.2920	24.33	21.49
9	572.2	0.3915	32.43	28.65
10	575.2	0.4361	38.26	33.79
11	577.2	0.5760	42.14	37.22
12	580.2	0.6454	43.10	38.06

$T_0 = 503.2 \text{ K}$; $H_0 = 6726 \text{ mJ}$; $\phi = 0.1683 \text{ }^\circ\text{C s}^{-1}$

TABLE 7

Data of 2,6-dinitrophenol determined by DSC with the sealed cell of stainless steel. Traces 3 and 4

Data point	T_i (K)	α_i	$(dH_i/dt)_i$ (mJ s ⁻¹)	$(d\alpha/dT)_i \times 10^3$ (K ⁻¹)
1	545.90	0.0166	2.182	1.822
2	554.15	0.0480	4.107	3.430
3	559.65	0.0578	6.042	5.045
4	563.90	0.0816	8.211	6.857
5	567.95	0.1134	10.93	9.126
6	572.15	0.1573	14.60	15.87
7	576.15	0.2134	19.00	19.85
8	579.65	0.2738	23.77	24.54
9	582.90	0.3457	29.39	29.66
10	585.55	0.4233	35.52	34.28
11	588.15	0.5102	41.05	34.28
12	590.75	0.6099	43.66	36.46

$T_0 = 524.65$ K; $H_0 = 6668$ mJ; $\phi = 0.1796$ °C s⁻¹

1	540.15	0.0188	2.035	1.694
2	548.65	0.0372	2.996	2.494
3	556.40	0.0656	5.118	4.260
4	563.40	0.0993	7.849	6.534
5	568.40	0.1449	11.37	9.467
6	573.40	0.1992	15.63	13.01
7	577.55	0.2576	19.54	16.27
8	580.40	0.3101	23.12	19.24
9	583.65	0.3816	28.44	23.67
10	586.40	0.4513	33.13	27.58
11	589.40	0.5327	37.74	31.41
12	591.65	0.6141	39.76	33.10

$T_0 = 514.40$ K; $H_0 = 6596$ mJ; $\phi = 0.1821$ °C s⁻¹

calculated value ($E = 169.5$ kJ mol⁻¹, $r = 0.9975$) obtained by Ozawa's method [5]. Similar computational results (see Tables 8–13) for samples IV (original data see Table 4), II (original data see Table 5) and I (original data see Tables 6 and 7), are not illustrated here one by one. The results of kinetic parameters of the above-mentioned energetic materials are all listed in Table 14.

Figure 5 shows a block diagram of the process of computing three kinetic parameters.

CONCLUSIONS

If kinetic data of a single non-isothermal DSC curve are analyzed by differential (eqn. (8)) and integral (eqn. (7)) methods, all the forms of $f(\alpha)$

TABLE 8

Results of analysis of the thermal decomposition data of double-base propellant by integral (eqn. (7)) and differential (eqn. (8)) methods

Func- tion No.	Integral method				Differential method			
	E (kJ mol ⁻¹)	$\log A$ (s ⁻¹)	r	Q	E (kJ mol ⁻¹)	$\log A$ (s ⁻¹)	r	Q
1	389.57	40.0	0.997	0.153859	352.07	35.8	0.992	0.320362
2	402.64	41.2	0.997	0.134292	371.65	37.8	0.992	0.235232
3	407.26	41.0	0.998	0.128888	378.59	37.9	0.995	0.209472
4	416.52	42.1	0.998	0.121353	392.30	39.4	0.997	0.168187
5	25.44	-ve	0.836	0.044804	46.99	2.33	0.962	0.028431
6	23.72	-ve	0.826	0.041974	43.20	1.98	0.943	0.037429
7	370.31	36.8	0.996	0.182561	325.35	31.8	0.988	0.438096
8	445.14	45.4	0.998	0.125970	433.59	44.2	0.998	0.114736
9	162.85	15.2	0.994	0.052932	163.51	15.4	0.996	0.035584
10	73.59	5.44	0.973	0.049450	88.57	7.17	0.992	0.020832
11	28.96	0.53	0.851	0.051138	54.68	3.44	0.983	0.016273
12	-ve	-ve	0.645	0.055111	24.31	0.07	0.939	0.013019
13	966.17	103	0.998	0.495714	937.83	100	0.998	0.544559
14	-ve	-ve	0.894	0.057955	10.66	-ve	0.799	0.011981
15	430.62	44.7	0.998	0.118238	412.82	42.8	0.998	0.128565
16	698.4	74.2	0.998	0.265832	673.63	71.4	0.998	0.297161
17	152.35	13.7	0.994	0.042087	144.84	12.9	0.990	0.065788
18	106.75	9.26	0.986	0.051128	58.40	3.90	0.674	0.657929
19	123.65	11.0	0.990	0.038996	91.28	7.47	0.895	0.331628
20	91.54	7.62	0.976	0.067514	28.69	0.66	0.328	1.101179
21	155.80	13.9	0.994	0.045007	151.03	13.5	0.993	0.052527
22	157.54	14.0	0.994	0.046718	154.13	13.7	0.994	0.047096
23	142.32	12.8	0.994	0.036929	126.53	11.1	0.977	0.124922
24	265.95	26.4	0.997	0.076655	236.16	23.1	0.989	0.204336
25	18.70	-ve	0.786	0.034683	32.07	0.87	0.827	0.076498
26	-ve	-ve	0.811	0.042263	6.83	-ve	0.345	0.062247
27	-ve	-ve	0.929	0.047614	4.90	-ve	0.546	0.545584
28	-ve	-ve	0.855	0.226550	201.75	19.7	0.995	0.060280
29	185.25	17.8	0.991	0.097092	201.75	19.7	0.995	0.060280
30	-ve	-ve	0.944	0.135792	182.5	17.2	0.997	0.033882

or $G(\alpha)$ should be used so as to single out the most probable general expression of $f(\alpha)$ or $G(\alpha)$ by the method of logical choice. By substituting this expression of $f(\alpha)$ into the exothermic rate equation (eqn. (12)), the corresponding values of E , A and n may be determined.

Equations (7), (8) and (12) are suitable for computer programming for fast computations.

TABLE 9

Results of analysis of the thermal decomposition data of 1,4,5,8-tetranitro 1,4,5,8-tetra-zadecalin by integral (eqn. (7)) and differential (eqn. (8)) methods

Func- tion No.	Integral method				Differential method			
	E (kJ mol ⁻¹)	$\log A$ (s ⁻¹)	r	Q	E (kJ mol ⁻¹)	$\log A$ (s ⁻¹)	r	Q
1	499.28	48.6	0.975	3.408301	496.71	48.3	0.983	2.246143
2	527.64	51.3	0.971	4.361546	544.07	53.0	0.979	3.314534
3	538.75	51.8	0.970	4.815237	562.84	54.4	0.976	3.980052
4	561.25	54.2	0.966	5.867469	598.96	58.2	0.971	5.658812
5	60.49	3.35	0.726	0.863867	128.21	10.3	0.945	0.508820
6	56.34	2.99	0.717	0.789531	116.17	9.21	0.958	0.310885
7	467.94	44.2	0.977	2.657792	452.95	42.6	0.984	1.680247
8	653.22	62.2	0.952	10.760357	707.75	69.8	0.951	13.881100
9	245.13	22.7	0.926	2.618090	312.75	29.8	0.945	3.041259
10	127.94	10.5	0.862	1.490356	204.31	18.5	0.931	0.168649
11	69.35	4.54	0.740	1.046374	152.33	13.1	0.917	1.143375
12	10.75	-ve	0.206	0.682314	102.88	8.01	0.894	0.698126
13	1299.84	131	0.970	27.153831	1348.28	136	0.970	29.890557
14	-ve	-ve	0.381	0.530256	79.53	5.54	0.873	0.515419
15	596.70	59.0	0.960	7.919443	652.53	64.9	0.961	9.097446
16	948.27	95.3	0.967	16.098023	999.30	100	0.967	18.053791
17	219.11	19.6	0.935	1.802018	260.86	23.9	0.967	1.207520
18	131.58	10.9	0.942	0.576677	29.66	0.35	0.145	10.758566
19	159.64	13.8	0.946	0.787591	113.13	8.94	0.720	3.122452
20	109.51	8.72	0.932	0.474659	-ve	-ve	-	-
21	227.41	20.3	0.932	2.032752	278.06	25.6	0.961	1.683292
22	231.69	20.6	0.931	2.162539	286.70	26.4	0.957	1.972058
23	196.42	17.4	0.941	1.295677	209.95	18.8	0.975	0.598644
24	347.85	33.0	0.966	2.225625	351.08	33.3	0.980	1.279116
25	44.99	1.92	0.680	0.618457	80.53	5.60	0.931	0.259863
26	-ve	-ve	0.131	0.448879	43.18	1.73	0.819	0.240324
27	-ve	-ve	0.631	0.374620	26.26	-ve	0.651	0.248628
28	4.52	-ve	0.039	3.473650	418.50	41.0	0.903	10.342634
29	307.37	29.3	0.900	0.580763	418.50	41.0	0.903	10.342634
30	-ve	-ve	0.595	1.242520	365.36	35.1	0.923	6.088878

TABLE 10

Results of analysis of the thermal decomposition data of 2,6-dinitrophenol by integral (eqn. (7)) and differential (eqn. (8)) methods. Trace 1

Func- tion No.	Integral method				Differential method			
	E (kJ mol ⁻¹)	$\log A$ (s ⁻¹)	r	Q	E (kJ mol ⁻¹)	$\log A$ (s ⁻¹)	r	Q
1	312.40	25.0	0.998	0.201199	305.14	24.3	0.998	0.150481
2	324.11	25.8	0.999	0.105319	323.74	25.8	0.999	0.036428
3	328.40	25.6	0.999	0.083051	330.58	25.8	0.999	0.034356
4	337.04	26.5	0.999	0.062642	343.96	27.1	0.999	0.096269
5	42.27	0.83	0.989	0.024762	64.54	2.88	0.976	0.127193
6	40.67	0.76	0.991	0.018353	60.14	2.55	0.983	0.079217
7	297.22	22.6	0.997	0.355075	283.59	21.3	0.996	0.364377
8	364.28	29.1	0.998	0.223438	384.19	31.0	0.996	0.803482
9	147.17	10.5	0.998	0.040923	166.48	12.3	0.992	0.296809
10	79.45	4.43	0.995	0.039488	103.46	6.67	0.980	0.276464
11	45.59	1.39	0.984	0.041970	73.38	3.95	0.963	0.261968
12	11.73	-ve	0.805	0.046588	45.06	1.37	0.916	0.243589
13	756.65	65.2	0.999	0.437916	766.98	66.2	0.999	0.599376
14	-ve	-ve	0.503	0.049696	31.88	0.14	0.855	0.233346
15	350.33	28.7	0.999	0.096446	363.90	30.0	0.998	0.347604
16	553.49	46.9	0.999	0.228765	564.92	48.0	0.998	0.440956
17	137.32	9.25	0.999	0.005817	147.19	10.1	0.997	0.059245
18	98.42	6.23	0.983	0.207287	55.54	2.28	0.705	1.944926
19	112.06	7.38	0.994	0.090923	90.86	5.43	0.949	0.564652
20	86.90	5.22	0.967	0.321524	23.74	-ve	0.278	4.189039
21	140.52	9.38	0.999	0.012344	153.60	10.6	0.996	0.116133
22	142.15	9.42	0.999	0.017442	156.81	10.8	0.995	0.152951
23	128.20	8.66	0.999	0.010777	128.11	8.67	0.998	0.023192
24	220.30	16.8	0.998	0.075754	215.54	16.4	0.998	0.062387
25	36.1	0.47	0.996	0.006268	47.05	1.47	0.992	0.019754
26	5.41	-ve	0.708	0.018202	23.59	-ve	0.968	0.023002
27	-ve	-ve	0.835	0.026687	13.06	-ve	0.898	0.025397
28	-ve	-ve	0.412	0.697572	205.54	16.0	0.975	1.370212
29	169.07	12.6	0.991	0.295176	205.54	16.0	0.975	1.370212
30	-ve	-ve	0.857	0.283497	185.95	13.8	0.983	0.734228

TABLE 11

Results of analysis of the thermal decomposition data of 2,6-dinitrophenol by integral (eqn. (7)) and differential (eqn. (8)) methods. Trace 2

Function No.	Integral method				Differential method			
	E (kJ mol ⁻¹)	$\log A$ (s ⁻¹)	r	Q	E (kJ mol ⁻¹)	$\log A$ (s ⁻¹)	r	Q
1	333.23	26.9	0.999	0.086250	319.99	25.7	0.999	0.080455
2	344.61	27.8	0.999	0.113440	337.99	27.2	0.998	0.167229
3	348.76	27.5	0.999	0.139907	344.59	27.2	0.998	0.245366
4	357.11	28.3	0.998	0.220098	357.50	28.4	0.996	0.469051
5	45.82	1.15	0.974	0.066509	62.94	2.76	0.958	0.203967
6	44.28	1.09	0.976	0.055092	58.74	2.45	0.967	0.140130
7	318.24	24.5	0.998	0.124732	298.67	22.7	0.998	0.136093
8	383.40	30.9	0.995	0.725478	396.31	32.2	0.990	1.710100
9	156.00	11.3	0.994	0.162876	168.97	12.5	0.983	0.559457
10	84.69	4.91	0.986	0.112984	102.82	6.63	0.966	0.435650
11	49.03	1.70	0.968	0.094563	71.37	3.80	0.942	0.373565
12	13.38	-ve	0.752	0.080494	41.97	1.12	0.876	0.311503
13	797.85	69.0	0.998	1.395091	801.22	69.4	0.997	2.197955
14	-ve	-ve	0.366	0.075091	28.42	-ve	0.792	0.281555
15	369.95	30.5	0.997	0.416982	376.74	31.2	0.994	0.975792
16	583.90	49.8	0.997	0.827709	588.43	50.2	0.996	1.514520
17	146.49	10.1	0.997	0.067004	150.39	10.5	0.992	0.191404
18	108.47	7.16	0.992	0.099099	61.79	2.87	0.755	1.687010
19	121.89	8.30	0.998	0.026874	96.05	5.94	0.964	0.411737
20	97.05	6.17	0.983	0.191209	30.45	0.06	0.350	3.892779
21	149.58	10.2	0.996	0.092660	156.56	10.9	0.990	0.289788
22	151.16	10.2	0.996	0.107741	159.66	11.0	0.988	0.348103
23	137.64	9.54	0.999	0.021127	132.00	9.06	0.997	0.042778
24	235.44	18.2	0.999	0.040015	224.83	17.3	0.999	0.053285
25	39.85	0.81	0.984	0.029591	46.26	1.43	0.984	0.039248
26	7.26	-ve	0.667	0.038490	21.70	-ve	0.936	0.038580
27	-ve	-ve	0.722	0.044080	10.79	-ve	0.798	0.039051
28	-ve	-ve	0.460	0.747822	206.58	16.1	0.963	1.948244
29	177.07	13.3	0.984	0.569559	206.58	16.1	0.963	1.948244
30	-ve	-ve	0.860	0.300999	187.71	14.0	0.973	1.145461

TABLE 12

Results of analysis of the thermal decomposition data of 2,6-dinitrophenol by integral (eqn. (7)) and differential (eqn. (8)) methods. Trace 3

Func- tion No.	Integral method				Differential method			
	E (kJ mol ⁻¹)	$\log A$ (s ⁻¹)	r	Q	E (kJ mol ⁻¹)	$\log A$ (s ⁻¹)	r	Q
1	349.22	27.8	0.996	0.266415	343.63	27.3	0.998	0.076285
2	363.41	28.9	0.996	0.300691	365.93	29.1	0.998	0.113442
3	368.56	28.7	0.996	0.322688	374.05	29.2	0.998	0.152831
4	378.89	29.7	0.995	0.381928	389.96	30.7	0.997	0.269269
5	46.21	1.19	0.964	0.049480	75.08	3.76	0.979	0.074336
6	44.29	1.10	0.966	0.042902	69.88	3.37	0.983	0.049384
7	330.20	25.1	0.996	0.265044	316.61	23.8	0.998	0.115718
8	411.30	32.7	0.993	0.709770	437.80	35.1	0.992	0.935352
9	165.03	11.9	0.990	0.160013	190.63	14.2	0.989	0.231114
10	88.47	5.17	0.981	0.090925	119.49	7.96	0.981	0.170785
11	50.18	1.80	0.960	0.065559	85.56	4.95	0.968	0.147789
12	11.89	-ve	0.695	0.046310	53.60	2.09	0.933	0.129821
13	854.19	72.6	0.995	1.883074	869.36	74.0	0.996	1.787744
14	-ve	-ve	0.541	0.038980	38.71	0.73	0.888	0.123116
15	394.75	32.1	0.994	0.514127	413.69	33.8	0.994	0.539201
16	624.47	52.3	0.995	1.088476	640.92	53.9	0.995	1.055483
17	123.27	10.5	0.993	0.100165	167.72	11.8	0.996	0.058595
18	105.44	6.78	0.986	0.094354	59.50	2.66	0.712	1.053708
19	122.49	8.21	0.993	0.062119	101.00	6.28	0.958	0.277830
20	90.77	5.52	0.973	0.138462	22.73	-ve	0.251	2.347839
21	157.10	10.7	0.992	0.116542	175.33	12.3	0.994	0.102600
22	159.05	10.7	0.991	0.126010	179.15	12.5	0.993	0.129672
23	142.27	9.78	0.994	0.068772	145.08	10.0	0.999	0.008036
24	245.75	18.8	0.996	0.148217	243.08	18.5	0.999	0.024326
25	38.79	0.74	0.970	0.028089	54.45	2.11	0.986	0.025387
26	4.30	-ve	0.444	0.023142	28.23	-ve	0.929	0.038651
27	-ve	-ve	0.835	0.022283	16.43	-ve	0.799	0.046826
28	-ve	-ve	0.410	0.389954	237.06	18.5	0.973	0.938601
29	190.88	14.3	0.982	0.400918	237.06	18.5	0.973	0.938601
30	-ve	-ve	0.877	0.149367	213.76	16.0	0.981	0.524683

TABLE 13

Results of analysis of the thermal decomposition data of 2,6-dinitrophenol by integral (eqn. (7)) and differential (eqn. (8)) methods. Trace 4

Func- tion No.	Integral method				Differential method			
	E (kJ mol ⁻¹)	$\log A$ (s ⁻¹)	r	Q	E (kJ mol ⁻¹)	$\log A$ (s ⁻¹)	r	Q
1	301.99	23.6	0.999	0.013256	302.13	23.6	0.999	0.037150
2	314.37	24.4	0.999	0.041378	321.65	25.1	0.998	0.094766
3	318.87	24.2	0.999	0.061344	328.76	25.1	0.998	0.142722
4	327.90	25.1	0.998	0.117143	342.70	26.4	0.997	0.277651
5	41.14	0.69	0.977	0.033880	69.63	3.20	0.970	0.125593
6	39.46	0.61	0.979	0.027719	64.98	2.86	0.975	0.091701
7	285.47	21.0	0.999	0.018380	278.61	20.4	0.999	0.053532
8	365.24	27.8	0.995	0.440462	384.60	30.3	0.992	1.013378
9	143.65	9.96	0.994	0.096167	170.51	12.3	0.987	0.327403
10	77.62	4.15	0.987	0.062794	108.64	6.93	0.975	0.253536
11	44.60	1.25	0.972	0.049203	78.96	4.30	0.961	0.217559
12	11.58	-ve	0.775	0.037677	50.80	1.77	0.925	0.182225
13	737.99	62.2	0.998	0.768161	756.78	63.9	0.997	0.127974
14	-ve	-ve	0.489	0.032687	37.58	0.56	0.885	0.165088
15	341.77	27.3	0.997	0.245839	363.48	29.3	0.994	0.579342
16	539.88	44.8	0.998	0.469828	559.66	46.6	0.996	0.894347
17	133.37	8.68	0.997	0.038879	150.35	10.2	0.993	0.121408
18	91.70	5.49	0.993	0.048899	54.56	2.14	0.743	1.020442
19	106.52	6.73	0.998	0.011094	91.43	5.36	0.964	0.269013
20	78.98	4.40	0.982	0.096307	21.61	-ve	0.281	2.311504
21	136.72	8.82	0.996	0.054292	157.05	10.6	0.991	0.176025
22	138.43	8.86	0.996	0.063313	160.41	10.8	0.990	0.208607
23	123.77	8.07	0.999	0.010781	130.39	8.66	0.997	0.042246
24	212.88	15.8	0.999	0.010451	215.28	16.0	0.998	0.039709
25	34.65	0.31	0.986	0.014236	51.18	1.75	0.981	0.042389
26	4.95	-ve	0.627	0.016082	27.91	-ve	0.942	0.041924
27	-ve	-ve	0.841	0.017135	17.34	-ve	0.867	0.041873
28	-ve	-ve	0.368	0.386909	211.32	16.1	0.971	1.116862
29	166.27	12.1	0.985	0.336725	211.32	16.1	0.971	1.116862
30	-ve	-ve	0.875	0.142409	190.85	13.9	0.979	0.659426

TABLE 14

Calculated values of kinetic parameters of thermal decomposition for some energetic materials

Energetic material	α	$G(\alpha)$	Eqn. (7)		Eqn. (8)		Eqn. (12)		
			E	$\log A$	E	$\log A$	E	$\log A$	n
I [6]	0.007–0.66	α	133 ± 8	9.01 ± 0.79	134 ± 8	9.10 ± 0.63	134 ± 9	9.17 ± 0.77	0
II	0.015–0.087	α	196	17.5	210	18.9	209	18.8	0
III	0.019–0.51	$1 - (1 - \alpha)^{1/2}$	177	16.4	178	16.5	180	17.0	0.54
IV	0.018–0.44	$-\ln(1 - \alpha)$	163	15.3	164	15.4	174	16.6	1.2

α , The fraction of material reacted; $G(\alpha)$, the integral mechanism function; E , the activation energy (kJ mol^{-1}); A , the pre-exponential constant ($1/s$); n , the reaction order.

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